

METHOD FOR PRODUCING PULP AND LIGNIN

Reference to Related Applications

- 5 This application claims the benefit of U.S. Provisional Application No. 60/474,961, filed June 3, 2003, and U.S. Provisional Application No. unassigned, filed October 6, 2003.

Technical Field

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This invention pertains to a method for producing pulp (comprising cellulose) and lignin from lignocellulosic material such as wood chips.

Background

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Wood is a composite material comprising cellulose, lignin and hemicellulose. Cellulose is the strong, fibrous component which consists of long chains of glucose molecules and which is used to make paper. Lignin is a phenolic polymeric matrix which holds the cellulose fibres together. Hemicellulose is the component com-
20 prised of short, branched chains of glucose and other like molecules.

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In general terms, pulping processes involve converting wood chips (or other suitable vegetative material) into a fibrous form in order to produce pulp. Pulp refers to cellulose fibres or material containing cellulose fibres which may be used
25 in the production of paper or paper containing products.

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The two main types of pulping processes in use today are mechanical pulping and chemical pulping though there are other pulping processes, such as chemi-thermal mechanical pulping, which are a combination thereof.

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Mechanical pulping involves the physical separation of individual fibres of the wood by forcing debarked logs and hot water between large rotating steel discs with teeth that tear the wood apart, or alternatively, by pressing logs against grindstones. Generally, pulps produced by mechanical pulping are of lower quality than pulps
35 produced according to chemical pulping, and thus are used to produce newsprint and cardboard type products.

On the other hand, chemical pulping involves subjecting wood to heat and chemicals in order to dissolve the lignin and hemicellulose binding materials, thereby

separating the cellulosic fibres. Kraft pulping is an example of a chemical pulping process, and involves cooking wood chips in a pressurized vessel known as a digester in the presence of hot caustic soda (NaOH) and sodium sulfide (Na₂S). Kraft pulping is a variation of the soda process where only NaOH is used to break
5 down and remove the lignin. Relative to the soda process, the addition of the sodium sulfide in the Kraft process assisted in dissolving the lignin with less damage to cellulosic fibres.

In Kraft pulping, the digestion process dissolves the lignin that "glues" the cellu-
10 losic fibers to each other in the wood. The resultant solution containing the dissolved ligneous material is referred to as a "black liquor". After digestion, the cellulose-containing pulp is separated from the black liquor and washed. At this stage, the resultant colored slurry of cellulose fibres is referred to as "brownstock". The color of the slurry is the result of some residual lignin remaining within the
15 slurry with the cellulosic fibres. If desired, a further step of bleaching the slurry can be carried out to remove some additional components of the lignin, thereby brightening the pulp. Typically, the pulp is bleached in multiple stages with various combinations of oxygen, hydrogen peroxide and sodium hydroxide. Chelation stages can be utilized in the bleaching process to remove transition metals
20 in the pulp which may otherwise interfere with peroxide bleaching.

One disadvantage with Kraft pulping is that it is carried out under extreme conditions which adversely affect yields. Kraft pulping typically involves pressures of approximately 120 p.s.i., temperatures of approximately 160 - 180 °C and initial pH
25 values over 12 in the digestion stage. In part, these reaction conditions are required by the fact that reactions carried out in Kraft pulping are oxidation reactions. These harsh conditions result in a loss of some cellulose and the destruction of much of natural form lignin from the wood chips.

Lignin typically is not recovered as an end-product in typical Kraft pulping processes. Instead, in Kraft pulping processes the black liquor is typically condensed in recovery boilers in the process of recovering chemicals such as sodium hydroxide for reuse. Solids such as lignin are burned as fuel to run the pulp mill utilizing the Kraft process. It would be advantageous to recover as much lignin as possible in a
35 pulping process since lignin is a valuable component in its own right, having a wide range of industrial applications such in the manufacture of fertilizers, asphalt

emulsifiers, soil stabilizers, wood products (such as plywood and particle board), oil well drilling fluids and dispersing agents for preparing concrete.

Summary of Invention

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In one aspect the invention provides for methods for producing pulp and lignin from lignocellulosic material, the pulp comprising cellulose. The methods comprise: (a) contacting the lignocellulosic material with an aqueous acid solution to impregnate the lignocellulosic material, the aqueous acid solution comprising from about 10%
10 to about 40% by weight of the acid; (b) heating the lignocellulosic material in two stages, the first heating stage being carried out for a period of time which is sufficient to depolymerize lignin within the lignocellulosic material without substantially degrading the cellulose or lignin in the lignocellulosic material, the second heating stage being carried out at or above the boiling point of the acid to distill off
15 the acid; (c) contacting the lignocellulosic material with an aqueous alkaline solution under heat to solubilize lignin in the alkaline solution, leaving a black liquor; (d) removing the pulp from the black liquor; (e) adding sufficient acid to the black liquor to precipitate the lignin; and (f) removing the lignin from the liquor.

20 The acid in step (a) may be nitric acid. The aqueous acid solution in step (a) may comprise, without limitation, from about 10% to about 30%, from about 15% to about 30%, from about 20% to about 25%, or from about 10% to about 15%, by weight of the acid.

25 The lignocellulosic material may be contacted with the aqueous acid solution in step (a) for at least 30 minutes, including without limitation, from about 12 hours to about 24 hours. The lignocellulosic material may be contacted with the aqueous acid solution in step (a) under heat. The lignocellulosic material may be contacted with the aqueous nitric acid solution in step (a) at a temperature from about 50 °C to
30 below the boiling point of the nitric acid.

The temperature during the second heating stage of step (b) may be, without limitation, from about 73 °C to below 100 °C or from about 90 °C to about 95 °C. The temperature during the first heating stage of step (b) may be, without limita-
35 tion, up to about 75 °C, from about 50 °C to about 75 °C, from about 60 °C to about 70 °C, from about 50 °C to about 60 °C, or from about 70 °C to about 75 °C. The first heating stage in step (b) may be carried out for at least 15 minutes.

The aqueous alkaline solution may comprise sodium hydroxide or potassium hydroxide or a combination of sodium hydroxide and potassium hydroxide. The aqueous alkaline solution may comprise an amount of alkali solute which is at least the normal equivalent of the nitric acid in the aqueous acid solution in step (a). The
5 aqueous alkaline solution may comprise an amount of alkali solute which is at least the molar equivalent of the nitric acid in the aqueous acid solution in step (a).

The acid used in step (e) may be sulfuric acid. The amount of acid added in step (e) may be at least the molar amount of the alkali in the aqueous alkaline solution in
10 step (c). The amount of acid added in step (e) may be at least the normal amount of the alkali in the aqueous alkaline solution in step (c).

The black liquor may cooled from the temperature in step (c) before the acid is added in step (e). The temperature of the black liquor when the acid is added in
15 step (e) may be, without limitation, up to about 75 °C, from about 5 °C to about 75 °C, from about 5 °C to about 50 °C, from about 25 °C to about 50 °C, or from about 50 °C to about 75 °C.

Any aqueous acid solution not absorbed by the lignocellulosic material in step (a)
20 may be removed prior to heating the lignocellulosic material in step (b). The methods may comprise collecting any aqueous acid solution which is removed prior to step (b) and recycling the collected aqueous acid solution for use in step (a), and comprising collecting any acid which is distilled off in step (b) and recycling the collected acid for use in step (a).

25 The starting moisture content of the lignocellulosic material may be from about 30% to about 55% by weight of water. The method may comprise contacting the lignocellulosic material with water before step (a) to increase the moisture content in the lignocellulosic material. The starting lignocellulosic material may comprise,
30 without limitation, wood chips, wood shavings, sawdust, pieces of rye, wheat, hemp and combinations of two or more of the foregoing. The starting lignocellulosic material may comprise undigested lignocellulosic material previously subjected to the method.

35 An amber liquor may be left following the removal of the lignin, and the method may comprise processing the amber liquor after the lignin has been removed, for example, to produce unicellular proteins or alcohols or both. Any water which is

produced as a reaction byproduct in one or more of the steps in the method may be collected and recycled for use in the method.

5 Steps (a) and (c) and the first heating stage in step (b) may each be carried out at a temperature from about 50 °C to about 75 °C. One or more of the heating of the impregnated lignocellulosic material in step (b), the contacting the lignocellulosic material with the aqueous alkaline solution in step (c) and the adding the acid in step (e) may be carried out with agitation. The methods may be carried out at atmospheric pressure.

10 The pulp removed in step (d) may be washed, pressed, bleached and dried. Similarly, the lignin removed in step (f) may be dried. Any residual liquor that is removed from the pulp by pressing may be collected and added to the black liquor prior to adding the acid in step (e). Similarly, any residual liquor which is removed
15 from the lignin during drying may be collected and added to the liquor after step (f), and wherein the liquor is processed after the lignin has been precipitated and removed.

20 Enough acid may be added to the solution in step (e) to lower the pH of the solution to an acidic pH.

Without limitation, step (c) may be carried out at a temperature up to about 75°C, from about 5 °C to about 75 °C, from about 50 °C to about 75 °C, from about 20 °C to about 50 °C, from about 30 °C to about 40 °C, or from about 40 °C to about 50
25 °C.

Step (a) may comprise immersing the lignocellulosic material in the aqueous acid solution in step (a), or spraying the lignocellulosic material with aqueous nitric acid solution.

30 In another aspect the invention provides for methods for producing pulp and lignin from lignocellulosic material, the pulp comprising cellulose, the methods comprise: (a) contacting the lignocellulosic material with an aqueous nitric acid solution to impregnate the lignocellulosic material, the aqueous nitric acid solution comprising
35 from about 10% to about 40% by weight of the nitric acid; (b) heating the impregnated lignocellulosic material in two stages, the first heating stage being carried out at a temperature from about 50 °C to about 75 °C for a period of time which is

sufficient to depolymerize lignin within the lignocellulosic material without substantially degrading the cellulose or lignin in the lignocellulosic material, the second heating stage being carried out at or above the boiling point of the nitric acid to distill off the nitric acid; (c) contacting the lignocellulosic material with an aqueous
5 alkaline solution at a temperature from about 50 °C to about 75 °C to solubilize lignin in the alkaline solution, leaving a black liquor, the aqueous alkaline solution comprising an amount of alkali which is at least the normal amount of the nitric acid in the aqueous acid solution in step (a); (d) removing the pulp from the black liquor; (e) cooling the black liquor and then adding an acid to the black liquor to
10 acidify the solution to precipitate the lignin; (f) removing the lignin, leaving an amber liquor; and (g) processing the amber liquor to produce unicellular proteins or alcohols or both, wherein any aqueous nitric acid not absorbed by the lignocellulosic material in step (a) is removed and collected following step (a) prior to heating the lignocellulosic material in step (b) and then recycled for use in step
15 (a), and wherein any nitric acid which is distilled off is collected prior to contacting the lignocellulosic material with the alkaline solution in step (c) and then recycled for use in step (a), and wherein the heating of the lignocellulosic material in step (b), the contacting the lignocellulosic material with the aqueous alkaline solution in step (c) and the addition of the acid in step (e) are each carried out with agitation.

20 In yet another aspect the invention provides for methods for producing pulp and lignin comprising the steps of contacting lignocellulosic material with an acid and, after removing any acid not absorbed by the lignocellulosic material, heating the lignocellulosic material at a temperature up to about 75 °C to effect the acid-
25 catalyzed hydrolytic depolymerization of the lignin in the lignocellulosic material without substantially degrading the cellulose or lignin in the lignocellulosic material, the acid-contacting and heating steps being carried out before the lignocellulosic material is digested in an alkaline liquor, the pulp being removed following the digestion of the lignocellulosic material in the alkaline liquor, the
30 lignin being removed after being precipitated out with the addition of an acid to the black liquor produced following the digestion of the lignocellulosic material in the alkaline liquor, wherein the pulp comprises cellulose. The acid-contacting step may comprise immersing the lignocellulosic material in an aqueous solution of the acid, and wherein the acid is nitric acid and the aqueous solution comprises from about
35 10 % to about 40 % by weight of nitric acid. The lignocellulosic material may be heated, after depolymerizing the lignin but before digesting the lignocellulosic

material, at a temperature above the boiling point of the acid in order to distill off the acid.

In yet another aspect the invention provides methods for treating lignocellulosic material comprising: (a) contacting the lignocellulosic material with an aqueous acid solution to impregnate the lignocellulosic material, the aqueous acid solution comprising from about 10% to about 40% by weight of the acid; (b) heating the lignocellulosic material in two stages, the first heating stage being carried out for a period of time which is sufficient to depolymerize lignin within the lignocellulosic material without substantially degrading the cellulose or lignin in the lignocellulosic material, the second heating stage being carried out at or above the boiling point of the acid to distill off the acid, wherein any aqueous acid solution not absorbed by the lignocellulosic material in step (a) is removed prior to heating the lignocellulosic material in step (b); (c) contacting the lignocellulosic material with an aqueous alkaline solution under heat to solubilize lignin in the alkaline solution, leaving a black liquor; and (d) removing the pulp from the black liquor, the pulp comprising cellulose.

In yet another aspect the invention provides methods for producing pulp and lignin from lignocellulosic material, the pulp comprising cellulose, the methods comprising: (a) contacting the lignocellulosic material with an aqueous nitric acid solution to impregnate the lignocellulosic material, the aqueous acid solution comprising from about 10% to about 40% by weight of the nitric acid; (b) heating the lignocellulosic material in two stages, the first heating stage being carried out for a period of time which is sufficient to depolymerize lignin within the lignocellulosic material without substantially degrading the cellulose or lignin in the lignocellulosic material, the second heating stage being carried out at or above the boiling point of the acid to distill off the acid, wherein any aqueous acid solution not absorbed by the lignocellulosic material in step (a) is removed prior to heating the lignocellulosic material in step (b); (c) contacting the lignocellulosic material with an aqueous alkaline solution under heat to solubilize lignin in the alkaline solution, leaving a black liquor; (d) removing the pulp from the black liquor; (e) adding sufficient acid to the black liquor to precipitate the lignin; and (f) removing the lignin from the liquor.

Further aspects of the invention and features of specific embodiments of the invention are described below.

Brief Description of Drawings

Figure 1 is an illustration of the mechanism of acid-catalyzed hydrolysis of an ester;
5 and

Figure 2 is a schematic illustration of a method according to the present invention.

Description

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Throughout the following description specific details are set forth in order to provide a more thorough understanding of the invention. However, the invention may be practiced without these particulars. In other instances, well known elements have not been shown or described in detail to avoid unnecessarily obscuring the
15 present invention. Accordingly, the specification and drawings are to be regarded in an illustrative, rather than a restrictive, sense.

Most existing pulping processes involve high pressure and/or high temperature conditions or concentrated chemicals. Not only do these factors increase costs, but
20 they also reduce the yield and purity of cellulose-containing pulp and lignin end-products since the cellulose and lignin can be degraded or destroyed during the pulping processes. The present invention addresses these deficiencies by utilizing the acid catalyzed hydrolysis of lignocellulosic material in methods for producing pulp and lignin from lignocellulosic material. The hydrolysis reaction allows the
25 controlled de-polymerization of lignin within the starting lignocellulosic material, utilizes much lower concentrations of pulping chemicals and lower temperatures than existing Kraft pulping processes and may be carried out at atmospheric pressure. These modest reaction conditions not only result in reduced costs relative to existing Kraft pulping processes, but also increase the yield and purity of the
30 cellulose-containing pulp and lignin since there is less degradation and and destruction of these components during the pulping process relative to existing Kraft pulping processes.

The invention includes methods involving contacting lignocellulosic material with
35 an acid, preferably nitric acid, in order to impregnate the lignocellulosic material and then heating the lignocellulosic material to de-polymerize the lignin within the lignocellulosic material prior to digesting the lignocellulosic material in an alkaline

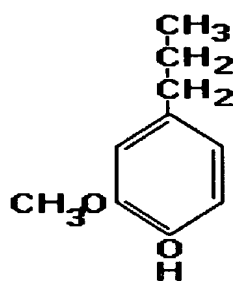
solution to solubilize lignin in the alkaline solution, leaving a black liquor (comprising the solubilized lignin) and pulp. The pulp is then removed and processed (e.g. pressing, washing, bleaching, drying). The solubilized lignin is precipitated out of the black liquor with the addition of an acid and then removed for processing. The
5 remaining solution can be further processed to produce other useful by-products such as unicellular proteins, alcohols or both.

As used herein, "lignocellulosic material" refers to any material which contains cellulose and lignin and, without limitation, includes pieces or particles (for
10 example wood chips, wood shavings, sawdust) from any type of tree (for example pine, oak, maple, fir, spruce) and other vegetative material (for example rye, wheat, hemp) and combinations thereof.

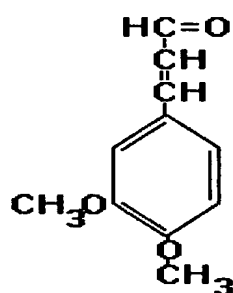
As used herein, "impregnation" refers to the absorption of an impregnating material
15 by lignocellulosic material. For example, impregnating wood chips can be accomplished by immersing or soaking the wood chips in a sufficient volume of the impregnating material (e.g. nitric acid solution) to saturate all or part of the wood chips. Other methods such as spraying could also be used to accomplish the
impregnation.

20 The separation of lignin and cellulose in their natural forms has proven difficult in practice. Many existing pulping processes are inefficient, with valuable cellulose and lignin being degraded, modified or destroyed during pulping, or less than optimal separation between cellulose and lignin being achieved in the pulping
25 process. The difficulty in separating lignin and cellulose arises from the inherent instability and fragile nature of pure lignin. Lignins are formed by removal of water from sugars to create aromatic structures and these reactions are irreversible. There are many possible monomers of lignin, and the types and proportions depend on the source in nature. Some typical monomers of lignin are shown below:

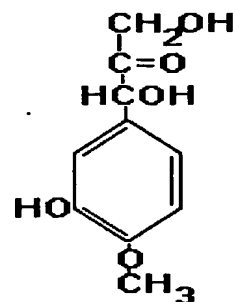
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(I)

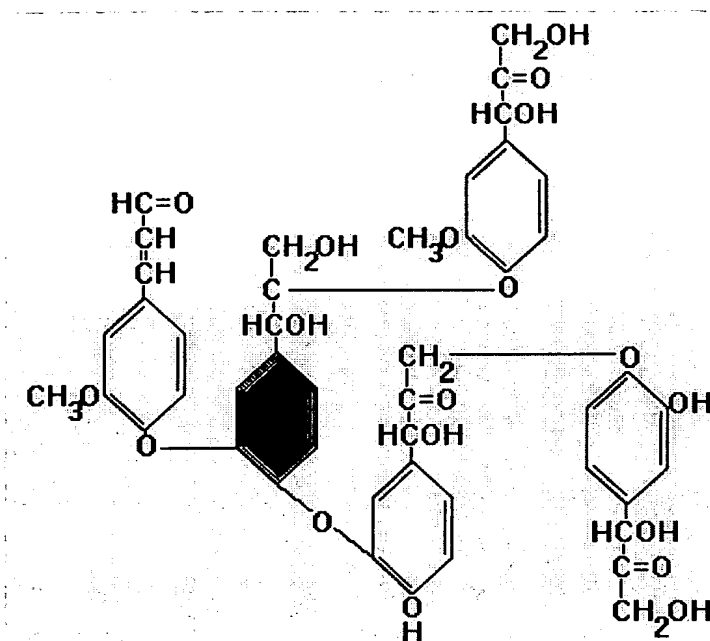


(II)



(III)

The hydroxyl (-OH) groups, either the hydroxyl groups on the chains or the
 5 hydroxyl groups on the aromatic rings, can react with each other or with the
 aldehyde or ketone groups. A ether linkage is formed when a hydroxyl group reacts
 with another hydroxyl group, a hemiacetal is formed when a hydroxyl group reacts
 with an aldehyde and a ketal is formed when a hydroxyl group reacts with a ketone.
 An early stage in the condensation of various monomers to form lignin is shown
 10 below, wherein there are several groups shown that can react further:



(IV)

Some monomers will simply extend the polymer while others will establish cross-linking. The shaded monomer has three of its functional groups linked to other monomers, so it is starting a branch or cross-link. Lignin molecules are three-dimensional and heavily cross-linked. A typical lignin molecule can have a molecular weight of about 15,000 amu. Lignin molecules are susceptible to harsh chemical concentrations and temperature exposure. A lignin polymeric matrix may be broken down at temperatures as low as 100°C. Lignin is unstable, light sensitive, and breaks down into acid compound as it ages, and its presence in paper items contributes to their degradation over time.

As mentioned above, the present invention utilizes the acid-catalyzed hydrolysis of lignocellulosic material. The lignin within lignocellulosic material includes ester functional groups. Figure 1 illustrates the mechanism of the acid-catalyzed hydroly-

sis of an ester. The rate of ester hydrolysis is very slow because their leaving groups are basic. The rate can be increased by the presence of a catalyst, such as an acid. In such an acid catalyzed reaction all organic reactants, intermediates, and products are positively charged. The following steps take place within the hydrolysis of the ester:

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- (A) An acid/base reaction is illustrated. Since there is only a weak nucleophile and a poor electrophile the ester needs to be activated. The acid protonates the ester carbonyl, making it more electrophilic.
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- (B) The oxygen atom in the water molecule functions as the nucleophile, attacking the electrophilic carbon atom in the $C=O$. Electrons move towards the oxonium ion, thereby creating a tetrahedral intermediate.
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- (C) Another acid/base reaction is illustrated. The oxygen atom in the water molecule is deprotonated to neutralize the charge.
- (D) Another acid/base reaction is illustrated. The $-OCH_3$ must leave, but first must be converted into a more stable group by being protonated.
- 20
- (E) The electrons from the adjacent oxygen atom assist the formation of the leaving group, a neutral methanol molecule CH_3OH .
- (F) Another acid/base reaction. The oxonium ion is deprotonated, which exposes the carbonyl $C=O$ carboxylic acid product and regenerates the acid catalyst.
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The carboxylic acid product obtained in (F) is a de-polymerized form of lignin. Because water (H_2O) and methanol (CH_3OH) have approximately the same basicity, it will be equally easy for the tetrahedral intermediates to collapse to reform the ester as it would be for the formation of the carboxylic acid. Hence, at equilibrium both the ester and the carboxylic acid will be obtained. However, an excess of water will shift the equilibrium towards the formation of the carboxylic acid product, de-polymerized lignin. Thus, methods of the present invention will render higher yields with the addition of water and, for this reason, it is possible to use

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35 lignocellulosic material which has a relatively high moisture content (e.g. "green" wood chips) or which has been previously contacted with water in order to increase

the moisture content prior to impregnating the lignocellulosic material with the acid.

The ability to use lignocellulosic materials with a relatively high moisture content in the present invention is an advantage compared to existing Kraft type pulping
5 processes. In many existing processes it is necessary to dry wood chips prior to pulping in order to remove or reduce moisture to meet stringent requirements. In fact, chips are preferred in many existing processes on a BDU (bone dry unit) basis. Requiring a drying step adds expense to such processes. The present invention overcomes this disadvantage since "wet" starting materials can be used, thus
10 removing the need to dry the wood chips or other starting materials. Moreover, as explained above in relation to Figure 1, since excess water drives the depolymerization reaction to favor the formation of a carboxylic acid instead of collapsing to reform an ester, additional moisture in the chips improves yields in methods according to this invention.

15 Following depolymerization of lignin, the lignocellulosic material is digested in the presence of an alkali such as sodium hydroxide (NaOH) and/or potassium hydroxide (KOH). The positive cations (K^+ or Na^+ or another suitable ion) then attacks the exposed -OH on the lignin product (carboxylic acid) bumping out the hydrogen
20 cation (H^+). The hydrogen cation then bonds with the negatively charged hydroxyl ion to form water. The lignin is then water-soluble and drops into solution, thereby separating the dissolved lignin from the cellulose-containing pulp. Due to more modest temperature, pressure and reactant concentrations involved, the lignin and cellulose produced are subject to less degradation than products obtained through a
25 Kraft type process, thereby providing increased yield and purity.

Figure 2 is a schematic illustration of a method 10 according to the present invention. Lignocellulosic material, such as wood chips (not shown), is used as the starting raw material in an impregnating tank 12. The wood chips are prepared by
30 chipping wood into a convenient size, for example, chips of roughly 0.5 - 2.0 inches in diameter. This can be done with a standard mill. Other sizes and shapes of lignocellulosic material can be used. Given the hydrolysis involved in the method, preferably "green" wood chips are used, or in other words, chips having a starting moisture content of approximately 30 - 55%, or even higher, by weight of
35 water. A pre-treatment stage could be utilized wherein the wood chips were immersed or otherwise contacted with water prior to being placed in the impregnating tank in order to increase the moisture content within the chips up to or beyond

30 - 55% by weight of water, though this step is not necessary to produce lignin, pulp and other ancillary products according to this invention. Impregnating bone dry chips with an acid solution could be done, but this will result in higher consumption rates of the acid impregnant, thereby increasing costs.

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Wood chips are loaded into impregnating tank 12 where they are contacted with an acid in order to impregnate the wood chips with the acid. The acid is preferably provided within an aqueous solution, and in such a case, the acid impregnates the wood chips as part of the solution. That is, the wood chips absorb both acid and
10 water. According to one aspect of the invention, the aqueous solution comprises from about 10% to about 40% by weight of the acid. The invention also includes utilizing other, narrower acid concentration ranges within this range. For example, the aqueous acid solution may comprise from about 15% to about 30%, from about 10% to about 25%, from about 10% to about 15%, or from about 20% to about
15 25%, by weight of the acid.

The aqueous acid solution is provided to impregnating tank 12 from acid solution tank 14 in a sufficient volume to immerse the wood chips. The acid used is preferably nitric acid, but those skilled in the art will appreciate that other acids
20 could instead be used within the scope of the present invention. Nitric acid is used herein for illustration purposes.

The wood chips are impregnated by allowing them to soak in the aqueous nitric acid solution in the impregnating tank 12. The impregnation time may last for as little
25 as 30 minutes or less and may extend for any length of time before the degradation of the wood chips begins to occur. For example, impregnation may last from about 2 hours and 45 minutes to about 48 hours. It is contemplated that the impregnation time may fall within a narrower time ranges such as, for example, from about 12 to about 24 hours and ranges within this range.

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Heating the chips during the impregnation step may decrease the impregnation time. For example, impregnation of the wood chips could occur from about 30 minutes or less to about 13 hours with the addition of heat, or up to 48 hours or longer, without the addition of heat. Heating during impregnation can be achieved by any
35 number of well known techniques that could be used to heat the wood chips within impregnating tank 12. For example, the exterior of impregnating tank could be heated with steam to heat the tank 12. After sufficient time has passed to complete

impregnation, any excess nitric acid solution is removed from the wood chips, by drainage for example, and passed to spent solution tank 16. Any collected excess nitric acid solution may then be recycled for use in the impregnating tank 12. Preferably any excess nitric acid solution is filtered and purified using conventional techniques before being reconstituted back up to strength. Filtration and/or purification could be accomplished by passing any spent nitric acid solution from spent acid solution tank 16 to a conventional filtration and/or purification apparatus (not shown) before the solution is passed to acid solution tank 14. However, it may not be necessary to filter and purify the excess nitric acid solution if there are not significant amounts of contaminants present.

The impregnated wood chips are then passed to a heating tank 18. This transfer can be accomplished by gravity feed, if impregnating tank 12 is located above the heating tank 18, or by a suitable transfer mechanism if not. The impregnated chips are heated within heating tank 18. The exterior of heating tank 18 is heated with steam produced by steam boiler 20, thereby heating the chips within heating tank 18. Many other known apparatus or techniques could alternatively be used to heat heating tank 18. Heating of the chips in heating tank 18 may be carried out in two heating stages; the first heating stage to depolymerize the lignin within the wood chips without substantially degrading the cellulose or lignin, and the second heating stage to distill off the acid following depolymerization of the lignin. The distilled off nitric acid is recycled for use in the impregnation stage. In particular, the distilled off nitric acid is collected and passed to a condenser 22 and then to spent solution tank 16 to be reconstituted to a desired strength and then passed back to nitric acid tank 14 for eventual use in impregnating tank 12.

The nitric acid attacks the cross-links or ester groups of the lignin polymeric matrix during the first heating stage. The first heating stage is carried out for a period of time which is sufficient to depolymerize the lignin within the wood chips without substantially degrading the cellulose or lignin. When nitric acid is used as the impregnating acid, preferably the first heating stage is carried out at a temperature up to about 75 °C, but above the freezing point of the aqueous acid solution. It is within the scope of the invention for the first heating stage to be carried out within a narrower temperature range, for example from about 50 °C to about 75 °C, from about 50 °C to about 60 °C, from about 70 °C to about 75 °C, or from about 60 °C to about 70 °C, when nitric acid is used as the impregnating acid. It is desirable to maintain these more modest temperatures (relative to Kraft pulping

temperatures) in order to prevent the unwanted degradation and destruction of the lignin and cellulose within the wood chips, thus providing improved product yield and purity.

- 5 Preferably heating tank 18 is fitted with an agitator 24 to provide agitation during the heating of chips within heating tank 18. Aggressive agitation by agitator 24 helps to both bring about a homogeneous temperature within heating tank 18 and to begin breaking apart the fibers in the wood chips.
- 10 During the second heating stage, the temperature is then brought above the boiling point of the acid for a sufficient time (for example, 30 minutes) to distill off the nitric acid. It is important to note that the temperature of the boiling point of the acid in this stage may depart slightly from the temperature that one would expect the acid to boil. This discrepancy results from various factors including the
- 15 interaction of the acid with the wood, the moisture content within the wood, and, for nitric acid, the formation of azeotropes with water. For example, whereas some scientific literature establishes the boiling point of nitric acid to be 83 °C, the inventor has observed boiling for nitric acid with wood chips as low as 73 °C. Thus, it is preferred for the temperature of the second heating stage within
- 20 heating tank 18 be at least about 73 °C where nitric acid is utilized. Similarly, it is also preferred to maintain the temperature during the second heating stage below the boiling point of water, 100 °C, to avoid the accidental distilling off of wood chip moisture, which would initiate the burning of the wood chips. Thus, according to one aspect of the invention, the second heating stage could be carried out from
- 25 about 73 °C to below 100 °C. Again, it is within the scope of the invention to utilize narrower ranges, for example from about 90 °C to about 95 °C, within this larger range.

- The amount of time for the first and second heating stages will vary depending upon
- 30 a number of factors, including the particular temperatures involved. For example, the first heating stage may be carried out for as little as 15 minutes, and could be carried out for a longer period of time.

- Following the heating in the heating tank 18, the wood chips are then transferred to
- 35 a digester 26. There the wood chips are digested by being contacted with a caustic solution, or in other words, an aqueous alkaline solution wherein the solute is an alkali such as sodium hydroxide, potassium hydroxide, or a combination of these.

Those skilled in the art will appreciate that other bases having similar chemical properties as these bases could be used. The wood chips are contacted with the aqueous alkaline solution under heat to solubilize the lignin in the solution. The resultant solution is darker in color due to the solubilized lignin and is thus referred to as black liquor. This digestion step thereby separates the lignin and the black liquor from the pulp. The alkaline solution is provided to digester 26 from caustic solution tank 28. The concentration of the alkaline solution is such to just make the lignin water soluble. This is accomplished by the positive cations (K^+ or Na^+ or another suitable ion) attaching to the exposed cleavage sites on the lignin monomers and the lignin then dissolving into the water.

The temperature during the digestion stage is preferably up to about 75 °C, but above the freezing point of the aqueous alkaline solution. It is however within the scope of the invention to increase the temperature above 75 °C up to the boiling point of the alkaline solution. For example, where the alkaline solution comprises an aqueous sodium hydroxide solution, it is possible for the temperature during the digestion step to be from about 75 °C to about 95 °C. It is also within the scope of the invention for the digestion stage to be carried out within a narrower temperature range, for example, from about 5 °C to about 75 °C, from about 50 °C to about 75 °C, from about 20 °C to about 50 °C, from about 30 °C to about 40 °C, or from about 40 °C to about 50 °C. Heat is provided to digester 26 by heater 30, which may be any conventional apparatus or arrangement for providing heat to the digester 26.

Digester 26 may be fitted with an agitator 32 to provide agitation during the digestion of the chips. Agitation helps to bring about a homogeneous temperature within the digester 26 and to break up the wood chips. Agitation also increases the rate that the cation (e.g. K^+ , Na^+ , etc.) binds to the exposed lignin cleavage sites thus minimizing any possible caustic action on the cellulose.

For cost and yield reasons, it is desirable to use as little alkali as possible within the caustic solution in the digestion of the wood chips. In one aspect of the invention, the alkaline solution may include an amount of alkali which is at least the normal equivalent of the nitric acid in the solution used in the impregnation stage. Adding excess alkali will increase costs by requiring more acid to be added at a later step. Further, the alkali concentration in the aqueous alkaline solution should be main-

tained below 17.5% by weight of the solution since beta and gamma cellulose dissolve at this level.

5 Following digestion, the resultant pulp (containing cellulose) and black liquor (containing solubilized lignin) is transferred to pulp tank 34 . The black liquor is removed, for example by drainage, and transferred to black liquor tank 36. The cellulose-containing pulp is then processed according to the user's needs. Typically, processing would involve washing, pressing, bleaching and drying the pulp following the separation from the black liquor. For example, in Figure 2, the
10 pulp would be pressed in a pulp press 38 to remove any residual black liquor (which would also be transferred to black liquor tank 36), and then bleached and dried with bleaching apparatus 40 and dryer 42. Bleaching apparatus 40 and dryer 42 could be any conventional known apparatuses for these purposes.

15 The lignin is precipitated out of the black liquor in black liquor tank 36 after the addition of an acid from acid solution tank 44. Preferably the acid added is a mineral acid, such as sulfuric acid. The acid added to the black liquor strips off the cation from the caustic solute, thereby precipitating out the lignin and a caustic salt (e.g. where sulfuric acid is used, the salts Na_2SO_4 , K_2SO_4 , or other similar salts
20 depending upon the alkali solute used in digestion, would result). Addition of the acid to the black liquor lowers the pH of the liquor until it is just slightly acidic. The acid may be added to the black liquor within an aqueous solution. For cost and yield reasons, it is advantageous if the acid solution is as dilute a solution as possible. Black liquor tank 36 may be fitted with an agitator 46 to provide agitation
25 during the addition of the acid from tank 44. The contents of black liquor tank 36 may be cooled, for example by cooler 48, in order to facilitate the precipitation of lignin. Cooler 48 can be any known apparatus for cooling purposes. The black liquor may be cooled from the digestion temperature before the addition of the acid. Preferably the temperature is up to about 75 °C, but above the freezing point of the
30 black liquor. Other narrower temperature ranges could be used at this step such as from about 5 °C to about 75 °C, 5 °C to about 75 °C, from about 50 °C to about 75 °C, or from about 25 °C to about 50 °C.

35 The precipitated lignin can then be removed from the resultant amber liquor (which is lighter in color than the black liquor due to the removal of the lignin) and processed using any conventional technique. For example, the resultant amber liquor and lignin slurry may be passed from black liquor tank 36 through a lignin

filter 50, with the lignin then being transferred to a lignin dryer 52 and dried at temperatures that will not degrade the lignin. The resultant lignin contains natural form lignin.

5 The filtrate passing through lignin filter 50 is the amber liquor, which is then transferred to an amber liquor tank 54. Any residual amber liquor removed during the drying of lignin in lignin dryer 52 is also transferred to amber liquor tank 54, as illustrated in Figure 2. Amber liquor is an aqueous solution containing starches, sugars, and other minerals and compounds found in plants that are not cellulose or
10 lignin. In amber liquor tank 54, the amber liquor can be processed to yield various other products of value including alcohols, unicellular proteins or both. For example, the amber liquor could be used as a starting culture for various bacteria to produce various products, such as animal feeds and alcohols. Amber liquor tank 54 may be fitted with an agitator 56 to provide agitation if desired. Any proteins
15 produced during the processing of the amber liquor may be removed by filtration (via protein filter 58) and dried (via protein dryer 60). Suitable apparatus modifications and/or additions could be made to accommodate alcohol processing and/or the production of other desired end products. The final filtrate can be recovered and treated in water treater 62 to remove any contaminants, thereby allowing the
20 recycling of water within various steps in the method, for example in reuse in washing in pulp tank 34, preparation of the alkaline solution in caustic solution tank 28 and in steam boiler 20. Any recovered water could also be used in steam boiler 20 or in the preparation of the aqueous acid solutions in acid solution tank 14 and/or acid solution tank 44.

25

Without limitation, the present invention provides the following benefits:

- 1) Wet starting materials can be used. Since water is essential to the hydrolysis of the lignocellulosic material, this removes the need to dry the starting
30 materials prior to the pulping process, thus resulting in lower costs relative to certain existing pulping methods.
- 2) The method of the present invention does not require added pressure, but may be carried out at atmospheric pressure. This reduces costs relative to
35 certain existing pulping methods, as does the fact that the method of the present invention does not require the addition of heat at temperatures approaching those used in typical Kraft type pulping processes.

- 3) Weak concentrations of strong acids and strong bases may be used, thereby minimizing raw material costs and degradation of final products.
- 4) The acid catalyst can be recovered and recycled for reuse, allowing improved cost efficiency. These factors also allow a closed system, minimize pollution, and therefore environmental impact. Very little pollution is caused by methods according to this invention.
- 5) Only small amounts of chemicals are needed to bring back to strength each recovered chemical before being reused in the method. Moreover, unlike recovery stages in certain Kraft type processes, external energy (and the resultant expense) is not required during the recovery of chemicals in methods according to the present invention.
- 6) Water used in the method may be recovered in saleable byproducts (such as alcohols and animal feeds) treated and reused or vented as steam, with suitable apparatus and process modifications. The vented steam could be used in providing energy for the method, thereby eliminating even this small loss of water.
- 7) The method is flexible in terms of starting materials. The ability to process a wide variety of lignocellulosic material without retooling any apparatus or changing the methods involved gives flexibility in pulp production. Currently, mills are typically designed to produce specific pulp types and utilize specific wood species as raw materials. Furthermore, most Kraft mills require chips meeting stringent quality specifications to remain economically viable. The present method may utilize not only any number of differently sized chips, but also sawdust, and also chips that would be considered "green" and unusable by current pulp mill standards. The flexibility provided by methods of this invention eliminates or simplifies the need for chip mills designed to produce chips of stringent standards, thereby offering the potential for lower operating and capital costs.
- 8) The yield of alpha cellulose is high using the method, while the method also allows for a high yield of lignin, which is a valuable component itself.

- 9) Aside from cellulose and lignin, other useful and potentially valuable by-products may be recovered using methods of this invention. For example, the amber liquor is suitable for fermentation of unicellular protein following precipitation and removal of lignin. The protein can be used in animal feeds or for research purposes.
- 10) Methods of the invention may be applied to different sized and configured apparatuses, thereby improving the flexibility of use.
- 11) Mills utilizing a method of the present invention will be highly efficient, with lower operating costs than mills using typical Kraft pulping processes.

The following examples are presented by way of illustration and not by way of limitation.

Example 1

This example comprises 19 trials which were run to illustrate the yields of pulp and lignin obtained using methods according to this invention, and also to illustrate the recovery of the acid used in the impregnation stage.

The starting lignocellulosic material in Trials 1 - 18 comprised 200 grams of a mixture of hardwood and softwood wood chips obtained from a sawmill and chip mill operation in Kelowna, British Columbia, Canada. 600 grams of wood chips were used as the starting material in Trial 19. All of the different species of trees that the chips originated from were not ascertained, but at least some of the chips came from Ponderosa Pine, Douglas Fir, Maple, Oak and Spruce.

The moisture content of the wood chips was between 35 - 50 % water by weight.

The moisture content was calculated by drying separate samples of the wood chips (which were not subjected to the steps of the method) and measuring the weight difference in the wood chips following the drying step.

The acid used in the impregnating step was nitric acid (HNO_3). Nitric acid solutions were prepared by diluting an amount (chosen depending upon the strength of solution desired) of 70% (w/w) nitric acid with distilled water. In each trial, 1 L of an aqueous nitric acid solution was used in the impregnating step, with the

exception that Trials 17 and 18 each used 750 mL, and Trial 19 used 2250 mL. A 2500 mL beaker sealed with laboratory film was used as the impregnating tank.

5 Following the impregnation step, excess nitric acid solution was removed from the wood chips before they were heated in the heating step. The heating step was carried out in a 2000 ml round bottom triple neck boiling flask, which was fitted with a distillation setup so that nitric acid distilled out in the heating step would be collected.

10 In order to calculate the efficiency of the method in recovering the nitric acid, samples from the excess acid solution collected following the impregnating step and from the distilled nitric acid which was collected during the heating step were each titrated using a 10% (w/w) % solution that was prepared by dissolving 100 g NaOH in distilled water and topped up in a 1 L volumetric flask. Titration of the excess
15 nitric acid solution collected from after the impregnation step permitted the calculation of the number of moles of nitric acid recovered after the impregnating step, which in turn permitted the calculation of the number of moles of nitric acid which were absorbed by the wood chips, since the moles of nitric acid in the initial 1 L solution was known. After titrating the nitric acid that was distilled out and
20 collected from the heating step, it was possible to calculate the total moles of nitric acid recovered in the method. By comparing this number to the amount of moles in a particular starting nitric acid solution allowed the calculation of the percentage of starting nitric acid which was recovered by the method. Also, it was found that red fuming nitric acid (RFNA) and nitrogen dioxide (NO_2) formed during the heating
25 step and these vapors were lost to the atmosphere. These vapors could have been retained with better equipment, and if that were the case, the amount of nitric acid actually recovered would have greatly increased. To account for this, the amount of mass lost from the heating tank was determined by weighing the tank before and after the heating stage, with the difference which was lost as RFNA and NO_2 . On
30 the assumption that this amount could be recoverable as HNO_3 with appropriate equipment modifications, it is then possible to calculate what the total moles of HNO_3 which would be recoverable using the method by adding the amount actually recovered with the amount lost as RFNA and NO_2 , and expressing this as a percentage of the starting moles of HNO_3 . This is shown in Tables 1-5 for Trials 1 - 19.
35 All titrations used 2 drops phenolphthalein as an indicator.

Following the heating step, the chips were digested in a round stainless steel tank with a 9.283 liter capacity (22.86 cm diameter, 11.43 cm height). The alkaline solution used in digestion was prepared by diluting an amount of 2.5 molar sodium hydroxide (NaOH) solution, 2.5 molar potassium hydroxide (KOH) solution, or a combination thereof, with distilled water. Various volumes of the initial 2.5 molar solutions were added to make the final alkaline solution used in digestion and various volumes of the final alkaline solution prepared were used for the various trials. The moles of each alkali solute(s) and the total volume of the aqueous alkaline solution prepared for Trials 1 - 19 are found in Tables 1 - 5.

10

In each of Trials 1 - 19 it took about 10 minutes or less to digest approximately 95% or more of the wood chips. In certain trials, a portion of the chips remained undigested, and the amounts are indicated in Tables 1 - 5 for such trials, as are the total digestion time for each trial.

15

Following the digestion step, the black liquor (containing solubilized lignin) was vacuum filtered in a buchner funnel without filter paper to remove the pulp, which was washed with distilled water and then air-dried at room temperature and weighed. The black liquor was transferred to a 2500 mL beaker, where the lignin was precipitated with the addition of a sulfuric acid (H_2SO_4) solution. The sulfuric acid solution was prepared by diluting an volume (depending upon the concentration sought) of pure sulfuric acid in a 1 L volumetric flask with distilled water. In most cases, the temperature of the black liquor was allowed to cool from the digestion step for the lignin precipitation step. The various temperatures are shown in Tables 1 - 5.

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The lignin was vacuum filtered in a buchner funnel without filter paper and thus removed from the amber liquor. The lignin was air-dried at room temperature and weighed. The lignin was not however dried and weighed for Trials 17 and 18. In these trials, the lignin did precipitate and was, by visual inspection, found to have a similar relative amount and appearance as the lignin produced in Trials 1 - 16.

30

As set out below, heat was applied during the heating and digestion steps and in five trials, during the impregnation step. Where so indicated, the heat was supplied in various steps by using a heating mantle made by Glas-Col Apparatus Co., Cat 10 0-410, having 465 total watts and 110 volts. The mantle controller was a Powerstat variable autotransformer, Type 3PN116B, made by The Superior Electric Co. of

35

Bristol, Conn. Agitation was provided during the digestion step by a cold steel impeller which was 8 inches in diameter with 1/2 inch separation between 45 ° offset blades. A 18 volt DEWALT™ XRP cordless drill was used to power the agitator. Agitation was provided during the lignin precipitation step by manual stirring using a glass stir rod for approximately 30 - 45 seconds in each trial.

The conditions and results of Trials 1 - 19 are found in Tables 1 - 5.

Table 1

		Trial 1	Trial 2	Trial 3	Trial 4
	IMPREGNATION STEP				
	% HNO ₃ (w/w)	15	24.15	25	30
	Impregnating Time (hours)	24	48	48	13
5	HEATING STEP				
	Time to reach 50 °C (min.)	55	41	40	30
	Time between 50 - 75 °C (min.)	76	91	30	75
	Time above 75 °C (min.)	59	19	35	32
	Minimum HNO ₃ Distillation Temp. (°C)	85	81	81	73
10	Distillation time (min.)	59	19	35	32
	DIGESTION STEP				
	Alkaline Solution				
	moles NaOH	0.425	0.625	0	0.435
	moles KOH	0	0.125	0.625	0.19
15	Vol. of Alkaline Solution (mL)	2670	3300	3000	3000
	Digestion Temp. (°C)	60	63	50	70
	Digestion Time (min.)	30	50	40	25
	Amount of Undigested Chips (g)	0	0	5.4	0
	LIGNIN PRECIPITATION STEP				
20	% H ₂ SO ₄ Solution added to black liquor (v/v)	20	10	10	20
	Vol. of Acid Sol'n added to black liquor (mL)	35	140	140	75
	Temp. during Addition of Acid (°C)	25	45	45	25
25	RESULTS				
	Pulp recovered (g)	92.1	104.6	99.6	94.5
	Pulp recovered (%)	46.05	52.3	49.8	47.25
	Lignin recovered (g)	41.4	42.1	39.8	43.1
	Lignin recovered (%)	20.7	21.05	19.9	21.55
30	HNO ₃ recoverable (%)	98.44	93.2	91.7	77.7

Table 2

		Trial 5	Trial 6	Trial 7	Trial 8
	IMPREGNATION STEP				
	% HNO ₃ (w/w)	15	15	11.5	15
5	Impregnating Time (hours)	24	21	48	13, at 75-80°C
	HEATING STEP				
	Time to reach 50 °C (min.)	15	19	31	35
	Time between 50 - 75 °C (min.)	20	90	65	25
	Time above 75 °C (min.)	45	12	15	20
10	Minimum HNO ₃ Distillation Temp. (°C)	83	81	83	83
	Distillation time (min.)	45	12	15	20
	DIGESTION STEP				
	Alkaline Solution				
15	moles NaOH	0.55	0	0.25	0.3125
	moles KOH	0	0.625	0.3	0.3
	Vol. of Alkaline Solution (mL)	3220	3250	3220	3245
	Digestion Temp. (°C)	50	50	60	70
	Digestion Time (min.)	30	60	15	30
20	Amount of Undigested Chips (g)	7	8.6	14.2	7
	LIGNIN PRECIPITATION STEP				
	% H ₂ SO ₄ Solution added to black liquor (v/v)	10	10	10	10
25	Vol. of Acid Sol'n added to black liquor (mL)	90	132	150	125
	Temp. during Addition of Acid (°C)	40	32	34	61
	RESULTS				
	Pulp recovered (g)	92.2	90.1	88.6	101.4
	Pulp recovered (%)	46.1	45.1	44.3	50.7
30	Lignin recovered (g)	37.9	39.1	38.3	42.2
	Lignin recovered (%)	19	19.6	19.2	21.1
	HNO ₃ recoverable (%)	93.4	92.1	93.4	88.1

Table 3

		Trial 9	Trial 10	Trial 11	Trial 12
	IMPREGNATION STEP				
	% HNO ₃ (w/w)	15	20	15	24.15
5	Impregnating Time (hours)	17 at 75-80 °C	2:45 at 75°C	31	30
	HEATING STEP				
	Time to reach 50 °C (min.)	35	19	37	41
	Time between 50 - 75 °C (min.)	24	85	32	105
	Time above 75 °C (min.)	22	12	114	30
10	Minimum HNO ₃ Distillation Temp. (°C)	83	75	80	83
	Distillation time (min.)	22	12	20	30
	DIGESTION STEP				
	Alkaline Solution				
15	moles NaOH	0.625	0.625	0	0.3125
	moles KOH	0	0	0.625	0.3125
	Vol. of Alkaline Solution (mL)	3000	3000	2500	2250
	Digestion Temp. (°C)	50 - 63	70	55	60
	Digestion Time (min.)	30	15	15	20
20	Amount of Undigested Chips (g)	0	20.3	24.4	0
	LIGNIN PRECIPITATION STEP				
	% H ₂ SO ₄ Solution added to black liquor (v/v)	10	10	20	10
	Vol. of Acid Sol'n added (mL)	150	150	65	125
25	Temp. during Addition of Acid (°C)	29	38	27	31
	RESULTS				
	Pulp recovered (g)	85.6	87.1	77.1	103.5
	Pulp recovered (%)	42.8	43.6	38.6	51.75
	Lignin recovered (g)	38.9	43.9	33.9	44.1
30	Lignin recovered (%)	19.5	22	17	22.05
	HNO ₃ recoverable (%)	93.4	92.61	93.8	65.05

Table 4

		Trial 13	Trial 14	Trial 15	Trial 16
	IMPREGNATION STEP				
	% HNO ₃ (w/w)	20	30	15	15
5	Impregnating Time (hours)	13	15	12	14
	HEATING STEP				
	Time to reach 50 °C (min.)	19	23	14	6
	Time between 50 - 75 °C (min.)	95	55	48	57
	Time above 75 °C (min.)	15	20	35	18
10	Minimum HNO ₃ Distillation Temp. , (°C)	81	80	81	79
	Distillation time (min.)	15	20	45	25
	DIGESTION STEP				
	Alkaline Solution				
15	moles NaOH	0.625	0	0.5	0.5
	moles KOH	0	0.625	0	0
	Vol. of Alkaline Solution (mL)	2500	2750	2700	2700
	Digestion Temp. (°C)	55	61	73	41
	Digestion Time (min.)	20	25	10	13
20	Amount of Undigested Chips (g)	4.9	11.6	28.7	102.3
	LIGNIN PRECIPITATION STEP				
	% H ₂ SO ₄ Solution added to black liquor (v/v)	10	10	20	20
	Vol. of Acid Sol'n added to black liquor (mL)	150	150	110	130
25	Temp. during Addition of Acid (°C)	26	36	18	5
	RESULTS				
	Pulp recovered (g)	96.4	87	71.2	35.2
	Pulp recovered (%)	48.2	43.5	35.6	17.6
30	Lignin recovered (g)	47	38.6	27.2	17.8
	Lignin recovered (%)	23.5	19.3	13.6	8.9
	HNO ₃ recoverable (%)	91.1	90.6	83.7	84.1

Table 5

	Trial 17	Trial 18	Trial 19
	IMPREGNATION STEP		
	% HNO ₃ (w/w)	15	15
5	Impregnating Time (hours)	1:25 at 50 - 55 °C	2:10 at 50 - 55 °C
	HEATING STEP		
	Time to reach 50 °C (min.)	12	20
	Time between 50 - 75 °C (min.)	60 (held between 70 - 75 °C)	35 (held between 60 - 70 °C)
10	Time above 75 °C (min.)	11	27
	Minimum HNO ₃ Distillation Temp. (°C)	83	83
	Distillation time (min.)	11	32
	DIGESTION STEP		
15	Alkaline Solution		
	moles NaOH	0.5	1.2625
	moles KOH	0	0
	Vol. of Alkaline Solution (mL)	2500	3050
20	Digestion Temp. (°C)	70	83
	Digestion Time (min.)	10	10
	Amount of Undigested Chips (g)	31.6	166
25	LIGNIN PRECIPITATION STEP		
	% H ₂ SO ₄ Solution added to black liquor (v/v)	20	20
	Vol. of Acid Sol'n added to black liquor (mL)	130	300
30	Temp. during Addition of Acid (°C)	7	32
	RESULTS		

	Pulp recovered (g)	71	67.6	169.3
	Pulp recovered (%)	35.5	33.8	28.2
	Lignin recovered (g)	Not Weighed	Not Weighed	72.5
	Lignin recovered (%)	Not Weighed	Not Weighed	12.1
5	HNO ₃ recoverable (%)	80.2	83.2	78.8

Example 2

10 This example comprised a trial that was similar to Trials 1 - 19 in example 1 except that the starting lignocellulosic material was 150 grams of shavings and sawdust from Hemlock, Oak and Pine tree species. Impregnation was done for 30 minutes in 15% (w/w) HNO₃ solution under heat of 50 °C. The impregnated shavings and sawdust were heated for 60 minutes between 50 - 75 °C, and then for 10 minutes over 80 °C. Following the heating step, the shavings and sawdust were contacted with an alkaline
15 solution having 1.25 moles of NaOH and 2600 mL total volume at a temperature of 52 °C for 7 minutes. Following pulp removal, lignin was precipitated with the addition of 20 % (v/v) H₂SO₄. The pulp and lignin were not weighed, but a visual inspection showed satisfactory appearance and yield for each, proving that the method of this invention can be carried out with relatively small pieces of lignocellulosic material
20 such as shavings and sawdust.

Example 3

25 The pulp samples produced in Trials 5, 7 and 2 from example 1 were subsequently analyzed to determine the relative amounts of alpha cellulose, beta cellulose and gamma cellulose therein. The results are found in Table 6 below.

30

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Table 6

	Trial 5	Trial 7	Trial 2
Alpha Cellulose (%)	81.3	79.6	79.2
Beta Cellulose (%)	4.4	3.7	7.5
5 Gamma Cellulose (%)	14.3	16.7	13.3

In addition to the methods herein, the present invention also includes pulp produced according to the methods herein, as well as paper products comprising cellulose from pulp produced according to the methods herein. Similarly, the present invention also includes lignin produced according to the methods herein, as well as numerous other products and compositions comprising lignin produced according to the methods herein, including for example, fertilizers, asphalt emulsifiers, soil stabilizers, wood products (such as plywood and particle board), oil well drilling fluids and dispersing agents for preparing concrete.

As will be apparent to those skilled in the art in the light of the foregoing disclosure, many alterations and modifications are possible in the practice of this invention without departing from the scope thereof. Accordingly, the scope of the invention is to be construed in accordance with the substance defined by the following claims.